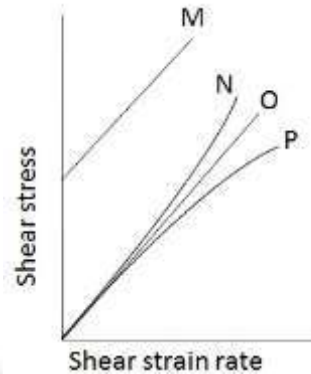


**XE (B): Q. 1 – Q. 9 carry one mark each & Q. 10 – Q. 22 carry two marks each.**

- Q.1 Rheological diagram of different types of fluids is shown in figure. Column I represents the nature of the fluid and column II represents the curve showing the variation of shear stress against shear strain rate.

Column I	Column II
(i) Newtonian	M
(ii) Shear thinning	N
(iii) Shear thickening	O
(iv) Bingham plastic	P



The most appropriate match between columns I and II is,

- (A) (i) – O; (ii) – N; (iii) – P; (iv) – M  
 (B) (i) – O; (ii) – P; (iii) – N; (iv) – M  
 (C) (i) – P; (ii) – O; (iii) – M; (iv) – N  
 (D) (i) – P; (ii) – O; (iii) – N; (iv) – M
- Q.2 In a two-dimensional, incompressible and irrotational flow, stream function ( $\psi = \psi(x, y)$ ) and velocity potential ( $\phi = \phi(x, y)$ ) exist. The velocities in x and y directions are non-zero.

The product of  $\left. \frac{dy}{dx} \right|_{\phi=\text{constant}}$  and  $\left. \frac{dy}{dx} \right|_{\psi=\text{constant}}$ , is

- (A) -1 (B) 0 (C) 1 (D)  $\infty$
- Q.3 The inviscid flow past a rotating circular cylinder can be generated by the superposition of
- (A) uniform flow, source and vortex (B) uniform flow, doublet  
 (C) uniform flow, sink and vortex (D) uniform flow, doublet and vortex
- Q.4 The velocity field and the surface normal vector are given by,  $\vec{V} = u\hat{i} + v\hat{j} + w\hat{k}$  and  $\vec{n} = n_1\hat{i} + n_2\hat{j} + n_3\hat{k}$ , respectively. If Euler equations are to be solved, the boundary condition that must be satisfied at the wall is,

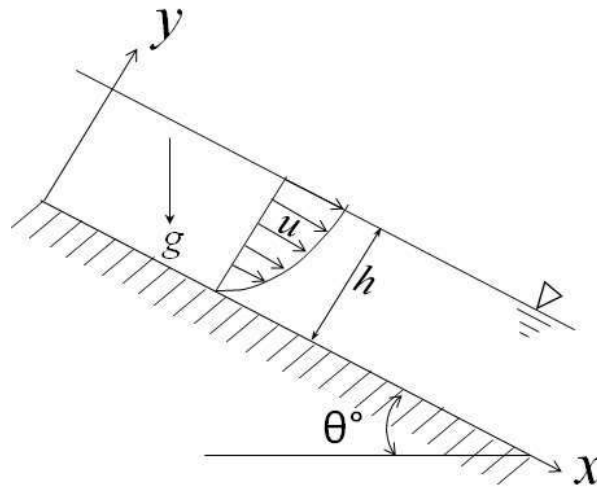
- (A)  $\vec{V} \cdot \vec{n} = 0$  (B)  $\vec{V} = 0$  (C)  $\nabla \cdot \vec{V} = 0$  (D)  $\vec{V} \times \vec{n} = 0$

- Q.5 The influence of Froude number is most significant in

- (A) capillary flows (B) creeping flows  
 (C) free surface flows (D) compressible flows

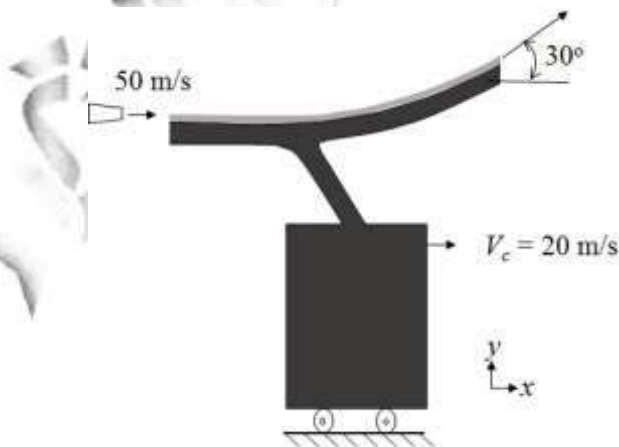
- Q.6 If the stream function ( $\psi(x, y)$ ) for a two-dimensional incompressible flow field is given as  $2y(x^2 - y^2)$ , the corresponding velocity field is
- (A)  $\vec{V} = 2(x^2 - 3y^2)\hat{i} + 4xy\hat{j}$   
(B)  $\vec{V} = 2(x^2 - 3y^2)\hat{i} - 4xy\hat{j}$   
(C)  $\vec{V} = 2(x^2y)\hat{i} - 4xy\hat{j}$   
(D)  $\vec{V} = 2(x^2y)\hat{i} + 4xy\hat{j}$
- Q.7 Water is flowing in two different tubes of diameters  $D$  and  $2D$ , with the same velocity. The ratio of laminar friction factors for the larger diameter tube to the smaller diameter tube is
- (A) 0.5 (B) 1.0 (C) 2.0 (D) 4.0
- Q.8 If the velocity field is  $\vec{V} = xy^2\hat{i} + 4xy\hat{j}$  m/s, vorticity of the fluid element in the field at  $(x=1, y=2)$  in  $s^{-1}$  is \_\_\_\_.
- Q.9 A pitot-static tube is used to measure air velocity in a duct by neglecting losses. The density of air is  $1.2 \text{ kg/m}^3$ . If the difference between the total and static pressures is 1 kPa, the velocity of air at the measuring location, in m/s, is \_\_\_\_.
- Q.10 A parallelepiped of  $(2 \text{ m} \times 2 \text{ m})$  square cross-section and 10 m in length, is partially floating in water upto a depth of 1.2 m, with its longest side being horizontal. The specific gravity of the block is
- (A) 0.8 (B) 0.6 (C) 0.5 (D) 0.4
- Q.11 The velocity field in a two-dimensional, unsteady flow is given by  $\vec{V}(x, y, t) = 2xy^2\hat{i} + 3xyt\hat{j}$  m/s. The magnitude of acceleration of a fluid particle located at  $x = 1 \text{ m}$ ,  $y = 1 \text{ m}$  at the time  $t = 1 \text{ s}$ , in  $\text{m/s}^2$ , is
- (A) 16.0 (B) 18.1 (C) 24.1 (D) 34.1
- Q.12 In a two-dimensional, incompressible and irrotational flow, fluid velocity ( $v$ ) in the  $y$ -direction is given by  $v = 2x - 5y$ . The velocity ( $u$ ) in the  $x$ -direction is
- (A)  $u = 2x - 5y$  (B)  $u = 2x + 5y$  (C)  $u = 5x + 2y$  (D)  $u = 5x - 2y$

- Q.13 A two-dimensional laminar viscous liquid film of constant thickness ( $h$ ) steadily flows down an incline as shown in figure. Acceleration due to gravity is  $g$ . If the velocity profile in the liquid film is given as,  $u = ky(2h - y)$ ;  $v = 0$ , the value of constant  $k$  is



- (A)  $\frac{\rho g \sin \theta}{2\mu}$  (B)  $\frac{\rho g \cos \theta}{2\mu}$   
 (C)  $\rho g \sin \theta$  (D)  $\rho g \cos \theta$

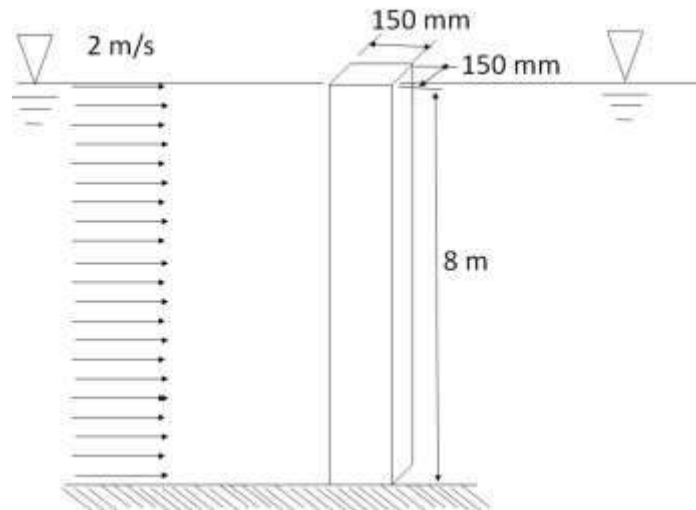
- Q.14 A water jet of 100 mm diameter issuing out of a nozzle at a speed of 50 m/s strikes a vane and flows along it as shown in figure. The vane is attached to a cart which is moving at a constant speed of 20 m/s on a frictionless track. The jet is deflected at an angle of  $30^\circ$ . Take the density of water as  $1000 \text{ kg/m}^3$ . Neglecting the friction between the vane and the fluid, the magnitude of the force exerted by water on the cart in the  $x$ -direction, in N, is \_\_\_\_\_.



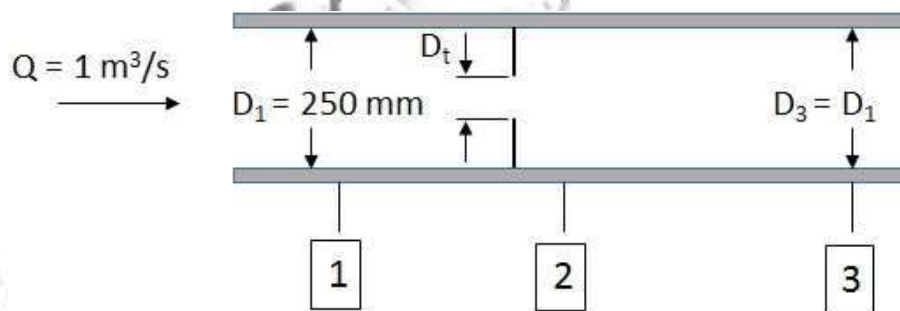
- Q.15 Capillary waves are generated in the sea. The speed of propagation ( $C$ ) of these waves is known to be a function of density ( $\rho$ ), wave length ( $\lambda$ ), and surface tension ( $\sigma$ ). Assume,  $\rho$  and  $\lambda$  to be constant. If the surface tension is doubled, in the functional form of the relevant non-dimensional group, the percentage increase in propagation speed ( $C$ ) is \_\_\_\_\_.

- Q.16 Consider a fully developed, two-dimensional and steady flow of a viscous fluid between two fixed parallel plates separated by a distance of 30 mm. The dynamic viscosity of the fluid is 0.01 kg/m-s and the pressure drop per unit length is 300 Pa/m. The fluid velocity at a distance of 10 mm from the bottom plate, in m/s, is \_\_\_\_\_.
- Q.17 A 2.6 gram smooth table-tennis (ping-pong) ball has a diameter of 38 mm. Density ( $\rho$ ) of air is 1.2 kg/m<sup>3</sup>. Neglect the effect of gravity. Take coefficient of drag as 0.5. If the ball is struck with an initial velocity of 30 m/s, the initial deceleration, in m/s<sup>2</sup>, is \_\_\_\_\_.
- Q.18 On a flat plate, transition from laminar to turbulent boundary layer occurred at a critical Reynolds number ( $Re_{cr}$ ). The empirical relations for the laminar and turbulent boundary layer thickness are given by  $\frac{\delta_{lam}}{x} = 5.48 Re_x^{-0.5}$  and  $\frac{\delta_{turb}}{x} = 0.37 Re_x^{-0.2}$ , respectively. The ratio of laminar to turbulent boundary layer thickness, at the location of transition, is 0.3. The value of  $Re_{cr}$  is \_\_\_\_\_.
- Q.19 In a capillary tube of radius  $R = 0.25$  mm, a fully developed laminar velocity profile is defined as,  $u = \frac{R^2}{4\mu} \left( -\frac{dp}{dx} \right) \left( 1 - \frac{r^2}{R^2} \right)$ . In this expression,  $-\frac{dp}{dx} = 1$  MPa/m,  $\mu$  is the dynamic viscosity of the fluid, and  $r$  is the radial position from the centerline of the tube. If the flow rate through the tube is 1000 mm<sup>3</sup>/s, the viscosity of the fluid, in Pa-s, is \_\_\_\_\_.
- Q.20 The skin friction coefficient for a turbulent pipe flow is defined as,  $C_f = \frac{\tau_w}{1/2 \rho V^2}$ , where  $\tau_w$  is the wall shear stress and  $V$  is the average flow velocity. The value of  $C_f$  is empirically given by the relation:  $C_f = 0.065 \left( \frac{2}{Re} \right)^{0.25}$ , where  $Re$  is the Reynolds number. If the average flow velocity is 10 m/s, diameter of the pipe is 250 mm, kinematic viscosity of the fluid is  $0.25 \times 10^{-6}$  m<sup>2</sup>/s, and density of the fluid is 700 kg/m<sup>3</sup>, the skin friction drag induced by the flow over 1 m length of the pipe, in N, is \_\_\_\_\_.

- Q.21 A  $(150 \text{ mm} \times 150 \text{ mm})$  square pillar is located in a river with water flowing at a velocity of  $2 \text{ m/s}$ , as shown in figure. The height of the pillar in water is  $8 \text{ m}$ . Take density of water as  $1000 \text{ kg/m}^3$  and kinematic viscosity as  $1 \times 10^{-6} \text{ m}^2/\text{s}$ . The coefficient of drag of the pillar is  $2.0$ . The drag force exerted by water on the pillar in N is \_\_\_\_\_.



- Q.22 An orifice plate is used to measure flow rate of air (density  $= 1.23 \text{ kg/m}^3$ ) in a duct of  $250 \text{ mm}$  diameter as shown in figure. The volume flow rate is  $1 \text{ m}^3/\text{s}$ . Flow at sections 1 and 3 is uniform and section 2 is located at vena contracta. The diameter ratio,  $D_t/D_1$ , is  $0.66$ . The flow area at vena contracta,  $A_2 = 0.65A_t$ , where  $A_t$  is area of the orifice. The pressure difference between locations 2 and 3 in  $\text{N/m}^2$  is \_\_\_\_\_.



**END OF THE QUESTION PAPER**